

SAFEN: SAFE Energy Carriers

2024-02-08

H2Cluster - H2 Market Meetup



A K E R H O R I Z O N S



STOREGDA

Agenda

1. SAFEN project overview (Thomas Welte)
2. SAFEN results (Ingar Fossan)

SAFEN Project Overview

SAFEN Joint Industry Project (JIP)

- Status:** JIP project started up in Q1 2022,
Phase 2 started in Q3 2023
- Schedule:** Phase 1 (1.5 years) + Phase 2 (2.5 years)
- Funding:** Industry partners and consultancies (in-kind)
- Project owner:** Safetec
- Partners:** Consultancies, Authorities, Energy companies /Asset owners

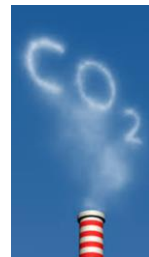


March 2022

Sept 2023

Des 2025

**Closing knowledge gaps,
sharing learnings and
developing risk-based methodologies
for hydrogen, ammonia and CCS facilities**



SAFEN partners

Project owner



Partners
Contractors



Partners



Authorities and
associated members



Technology
providers



Safety challenges in the hydrogen, ammonia and CCS value chain

Maritime

Need to prove that alternative solution is as safe as conventional technology



Alternative

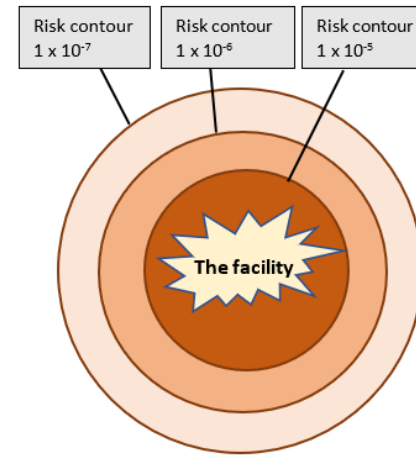


Conventional



Land based production facilities

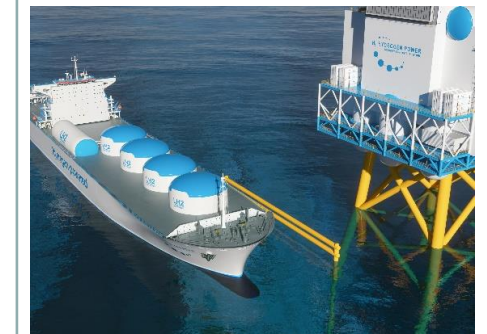
Storage of large amounts of H₂, NH₃ and CO₂



SAFEN will deliver the basis for assessing what is safe enough!

Loading, bunkering and refuelling operations

High transfer rates
Human operations



Knowledge

- Quantitative data and statistics
- Qualitative data and understanding of failure mechanisms

Models

- New and improved models for:**
- Loss of containment (LoC) frequency
 - Ignition probability

Recommendations

- Recommendations for application of SAFEN results (models, design, risk management, ...)**

Impact

- **Cost-efficient safety design**
- **Safe and sustainable renewable installations and energy system**

SAFEN and HICON

- Safetec has been granted funding from the Research Council of Norway for the proposed innovation project “HICON – Hydrogen Ignition CONtrol”



Prosjek

HJEM | NYHETER OG PRESSEMELDINGER | 216 MILLIONER TIL FORSKNING PÅ FORNYBAR ENERGI

216 millioner til forskning på fornybar energi

Forskningrådet investerer i 25 nye prosjekter innen fornybar energiproduksjon, energibruk og kraftsystemet. Alle prosjektene ledes av bedrifter.

PRESSEMELDING | PUBLISERT 18. DES 2023

DEL | LAST NED

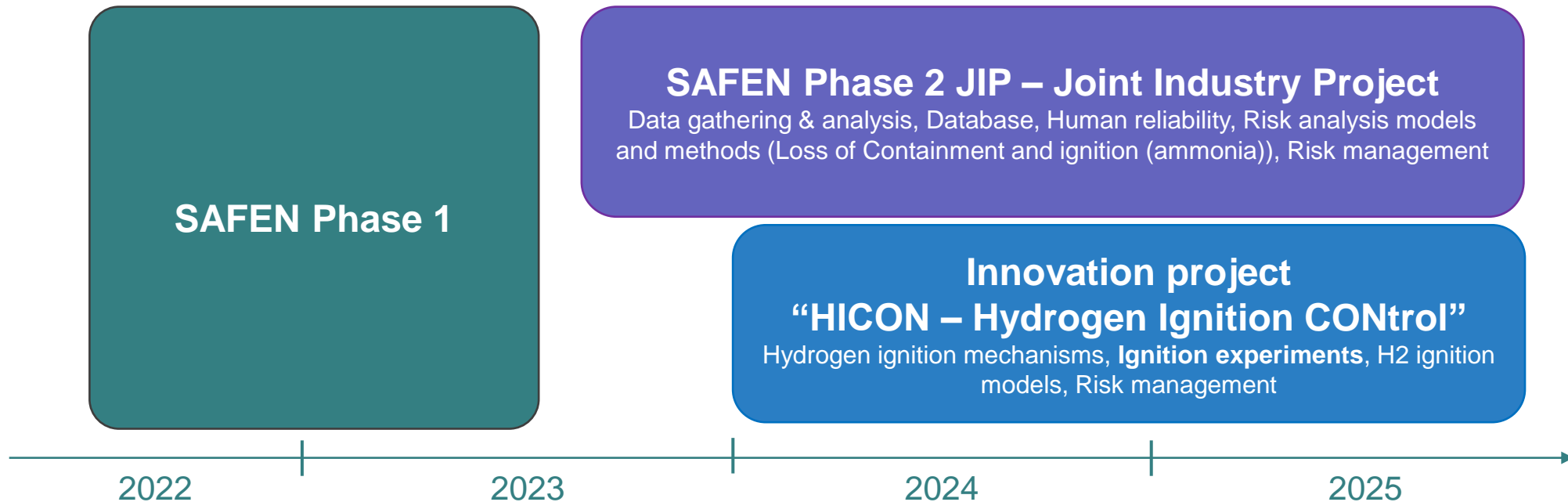
DISSE FÅR STØTTE:

Bedrift	Prosjekttittel	Innstilt beløp (i 1000)	Fylke	Kommune
SAFETEC NOR-DIC AS	Hydrogen Ignition CONtrol	6 450	Trøndelag	Trondheim

[216 millioner til forskning på fornybar energi \(forskningradet.no\)](https://forskningradet.no)

SAFEN Phase 2 project structure

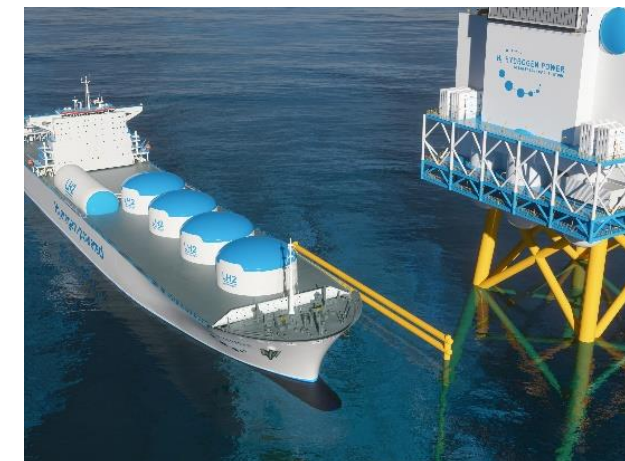
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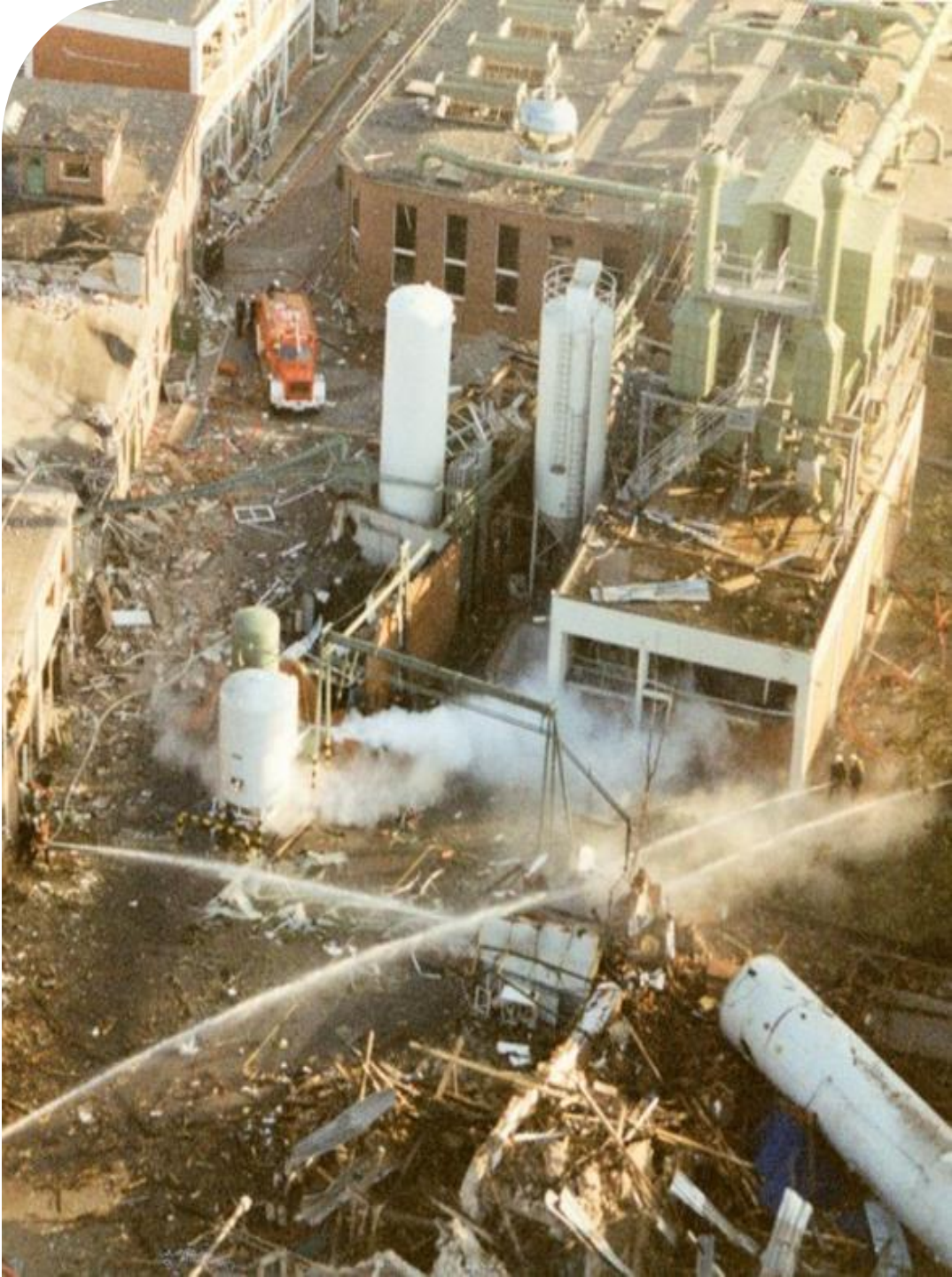
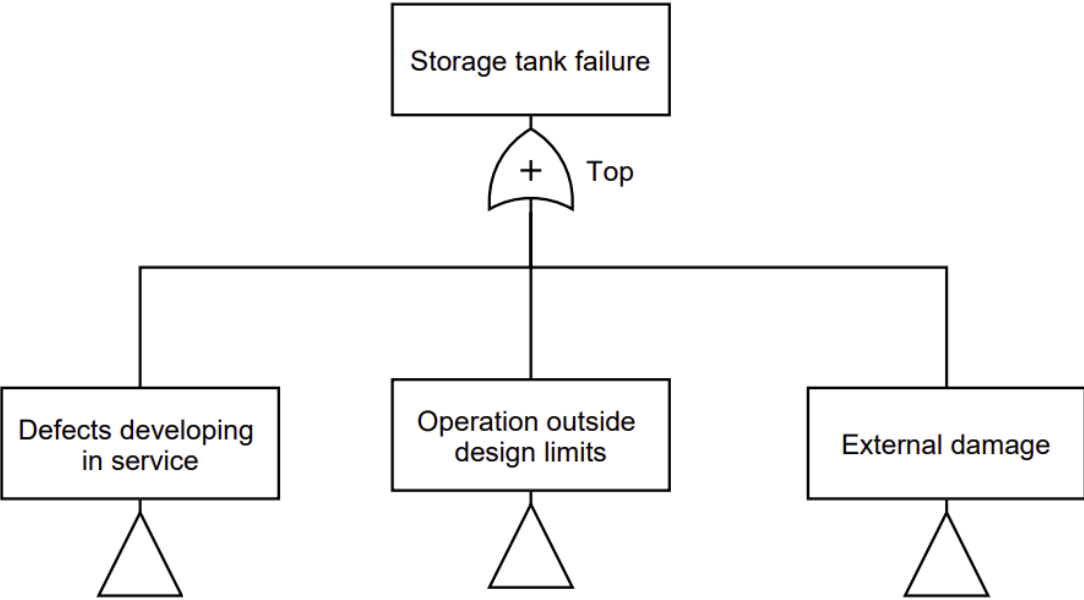
SAFEN Results

SAFEN models

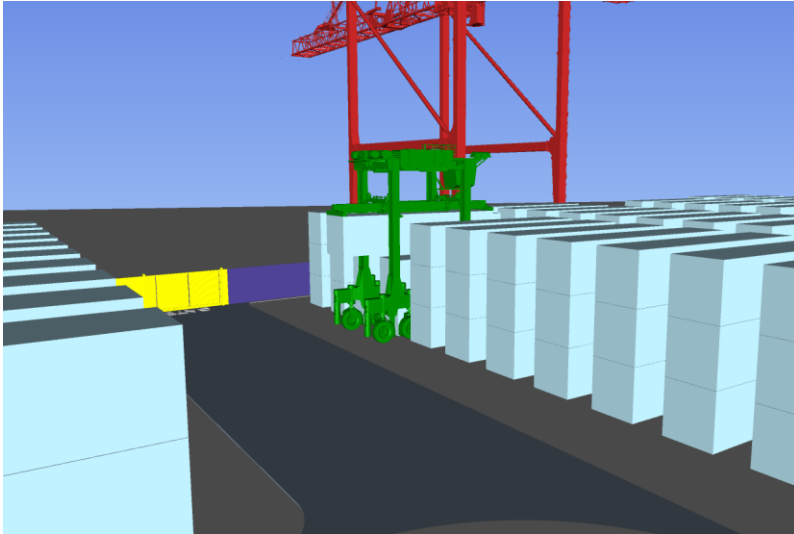
- Storage tanks
 - Simple LoC model with guidelines
- Process equipment
 - New LoC model
- Transfer operations
 - SAFEN support further development of new RIVM model
- Ignition probability models
 - Hydrogen
 - Ammonia (on-going)



Storage tank failure



Many identical items



Containerized storage solutions
(permanent or mobile)



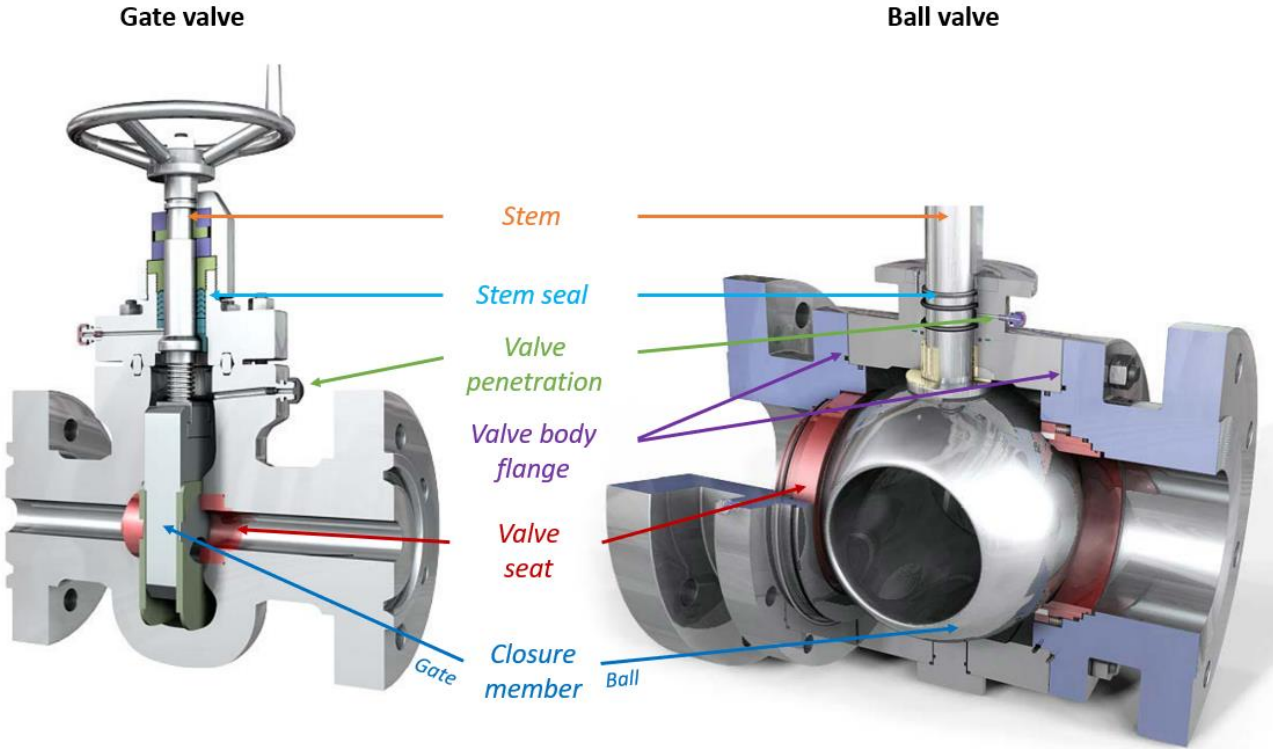
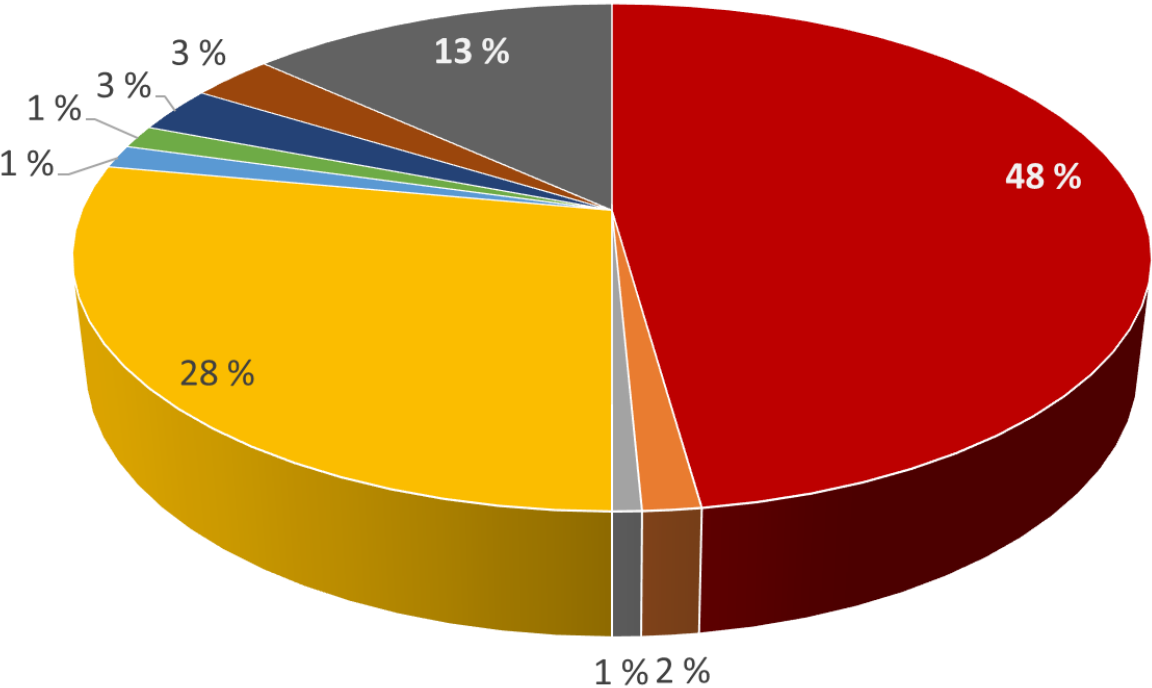
Transport modules

What is the frequency for rupture scenarios for such a design, can we extrapolate from existing models; 63 tanks · $X \cdot 10^{-y}$ ruptures per tank/year?

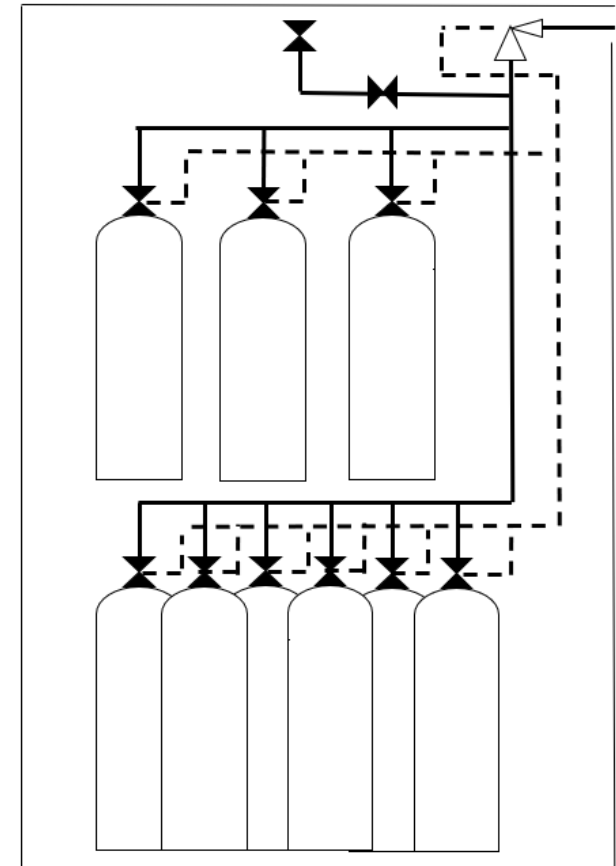
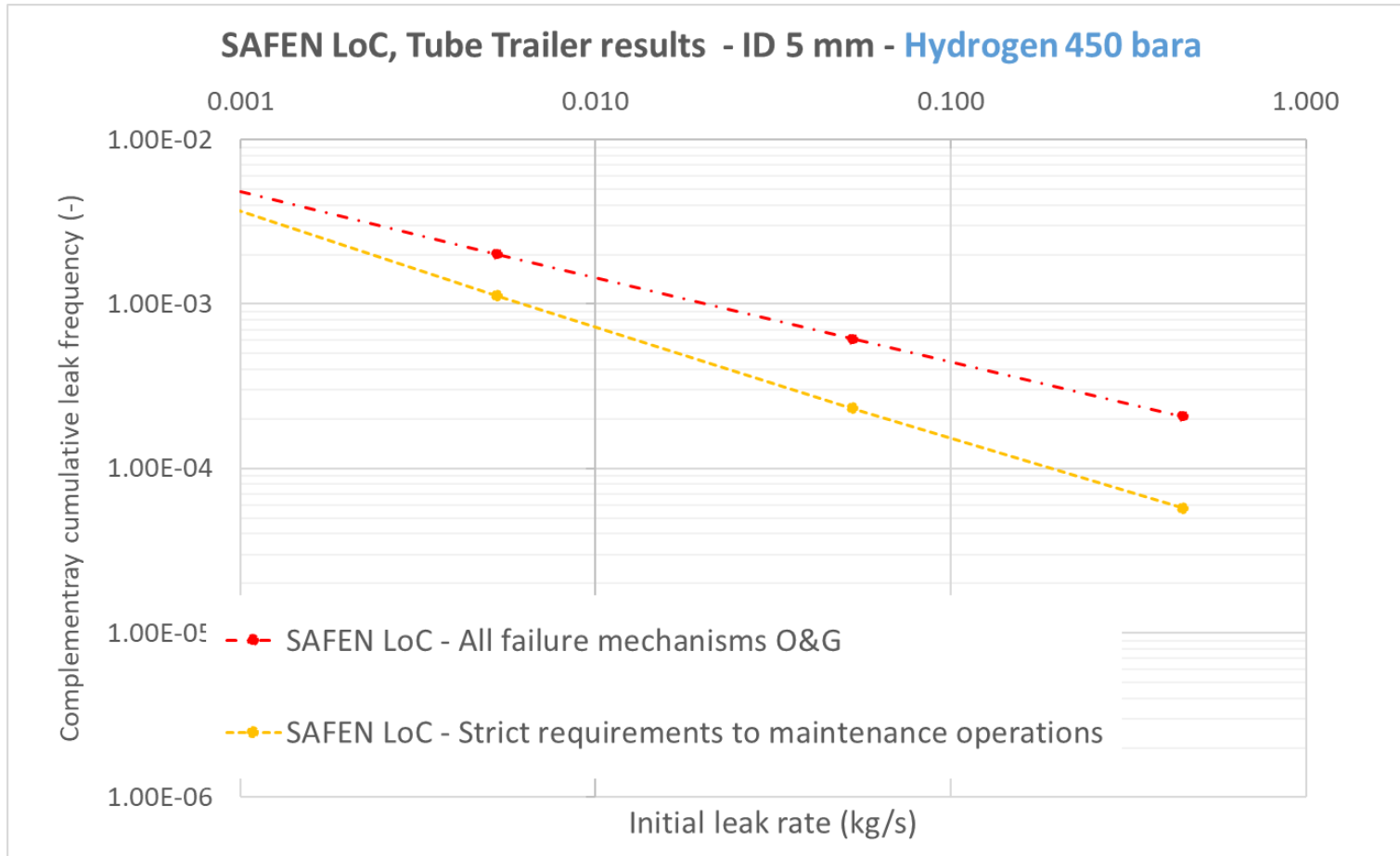
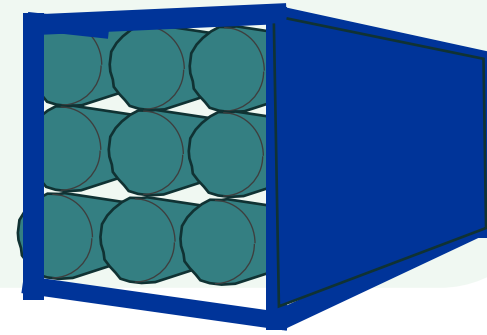
It is about operation and not about technical integrity!

Valve in erroneous position causing unintentional flow is the main driver for leaks related to valves

- Closure member
- Stem
- Stem seal
- Unknown
- Valve body
- Valve body flange
- Valve detached
- Valve penetration

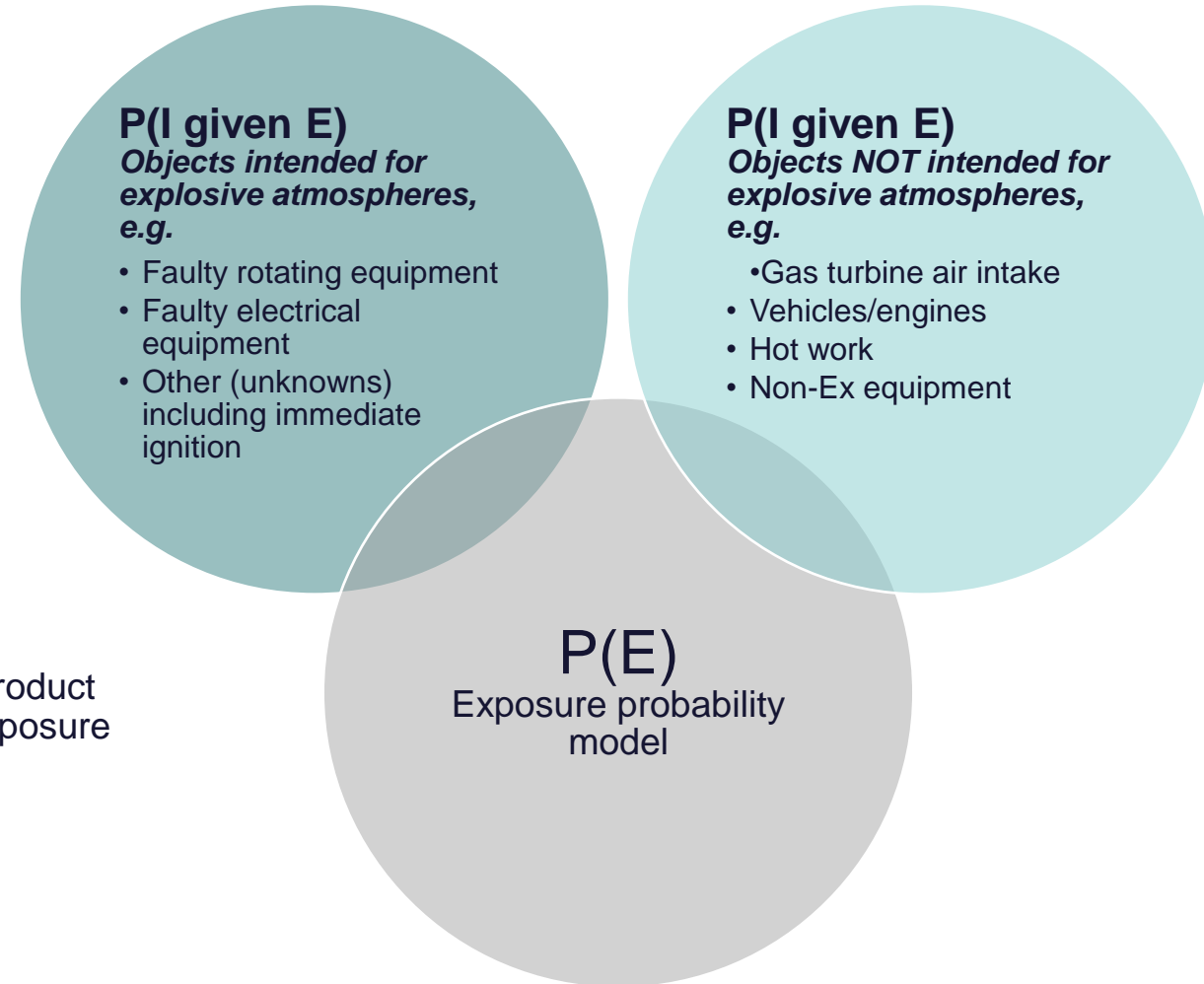


Which failure mechanisms count?

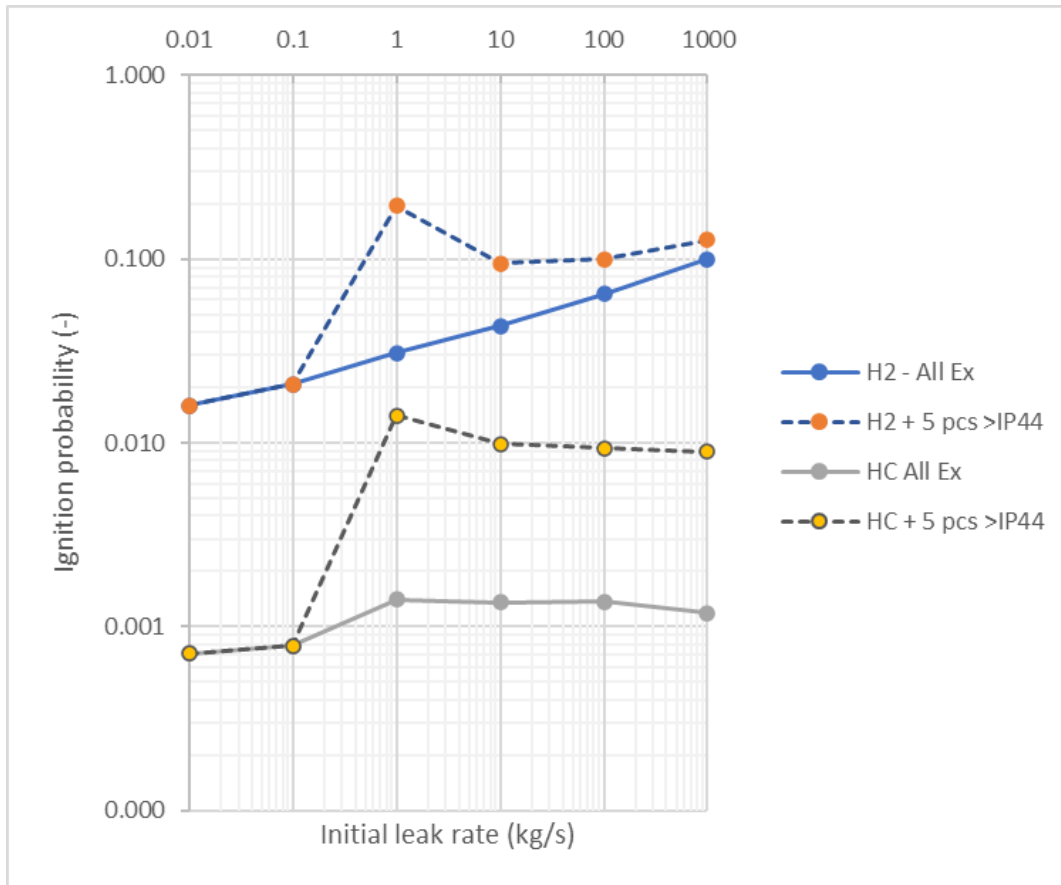
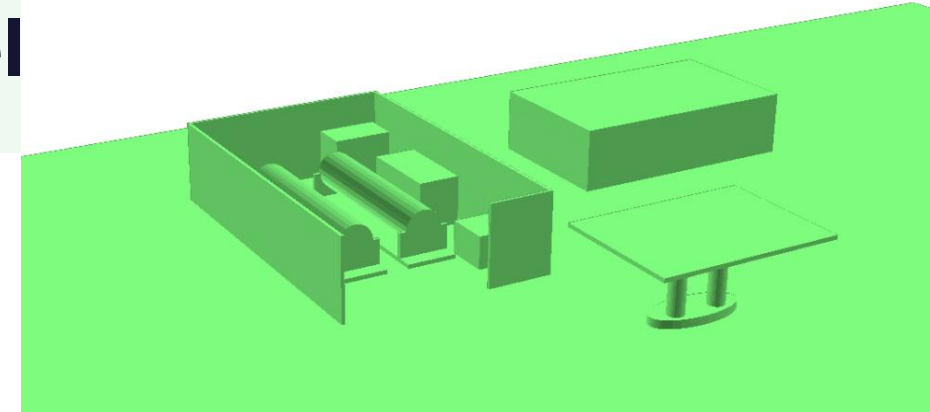


SAFEN Ignition model

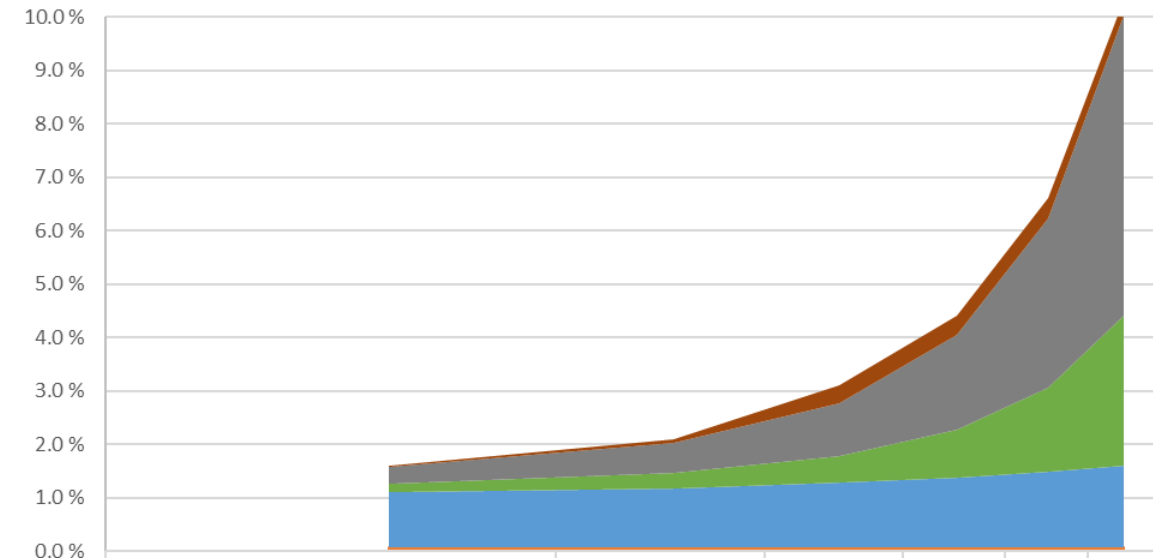
- The properties of the ignition control barrier matters
 - type of ignition sources
 - isolation of equipment
 - detection
 - etc
- The size of the combustible cloud play a role – the likelihood for exposure to a live ignition source
- Our hypothesis therefore that we should develop a model in line with the rationale for MISOF model HC: the ignition probability is the product of the probability for exposure and the probability for ignition given exposure
- But we need to include parameters reflecting
 - Ignition by hot surfaces
 - Ignition by electrostatic discharges
 - Ignition by corona discharges
 - Adiabatic compression and shock waves(diffusion ignition)
 - Ignition of LH2 releases in/onto water (not implemented yet)



SAFEN H2 ignition probability model



Small H2 fuelling station with 100 m3 processing area - all Ex equipment



	0.01	0.1	1	10	100	1000
Delayed (Electrostatic + Hot surface)	1.5E-04	7.0E-04	3.2E-03	3.5E-03	3.7E-03	2.8E-03
Electrostatic discharges	3.2E-03	5.6E-03	1.0E-02	1.8E-02	3.2E-02	5.6E-02
Mechancial impact	1.6E-03	2.8E-03	5.0E-03	8.9E-03	1.6E-02	2.8E-02
Diffusion total	1.0E-02	1.1E-02	1.2E-02	1.3E-02	1.4E-02	1.5E-02
Generic immediate	7.0E-04	7.0E-04	7.0E-04	7.0E-04	7.0E-04	7.0E-04

Interested to learn more about SAFEN, and how you can benefit from the project?



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